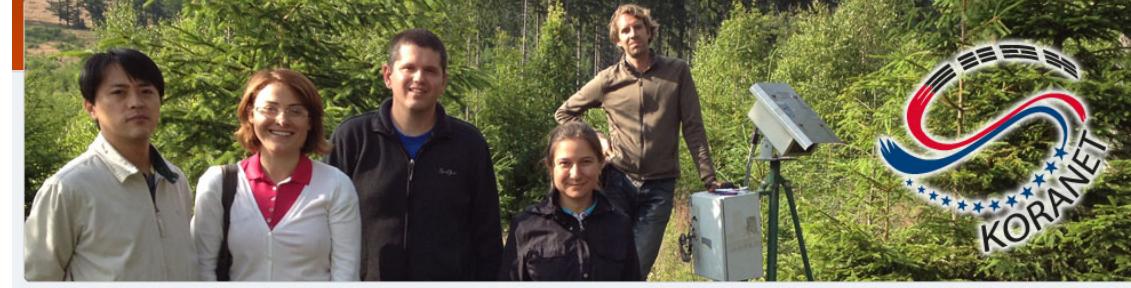




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Carbon
Materials
Processing
Group
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Pyrolysis - Sustainable waste treatment with negative carbon balance

Esin Apaydın-Varol & Başak Burcu Uzun

Anadolu University, Dept. of CHEMICAL Eng., Eskisehir, TURKEY



OUTLINE

- Objective-Motivation
- Biomass
- Thermochemical Conversion Processes
 - Pyrolysis
- Pyrolysis Products
 - Bio-oil
 - Bio-char
- Conclusion



OUTLINE

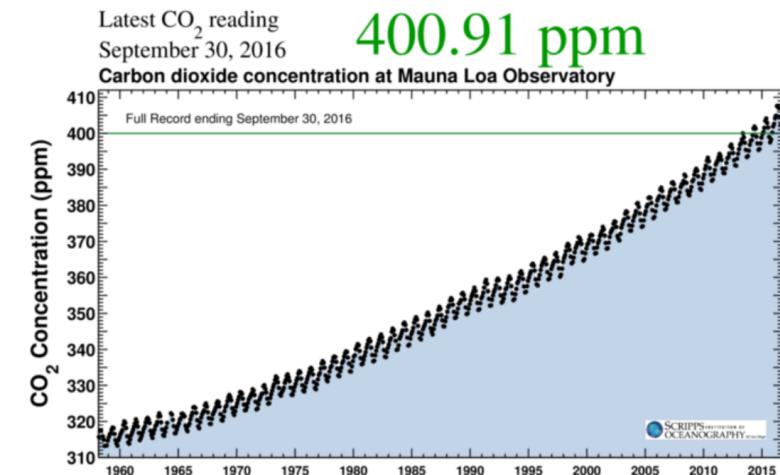
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Objective-Motivation

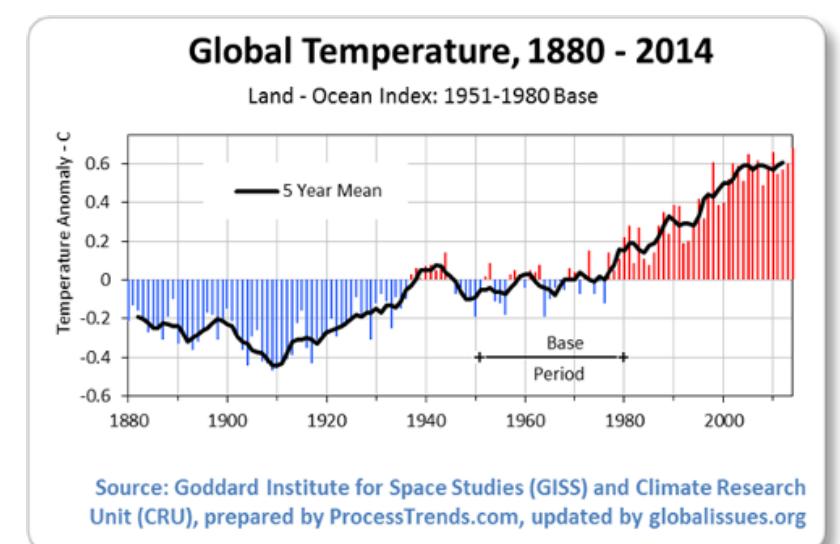
According to WHO:

- Over the last 50 years, human activities have released sufficient quantities of CO₂ and other greenhouse gases to trap additional heat in the lower atmosphere and affect the global climate.
- In the last 130 years, the world has warmed by approximately 0.85°C. Each of the last 3 decades has been successively warmer than any preceding decade since 1850.
- Sea levels are rising, glaciers are melting and precipitation patterns are changing. Extreme weather events are becoming more intense and frequent.

<http://www.who.int/mediacentre/factsheets/fs266/en/>



Atmospheric carbon dioxide concentrations, recorded by the Mauna Loa Observatory in Hawaii. The line is jagged because CO₂ levels rise and fall slightly each year in response to plant growth cycles. Scripps Institute of Oceanography





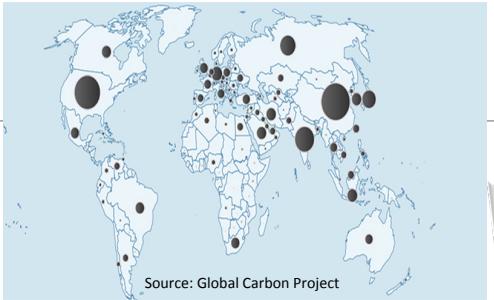
Objective-Motivation



*Increasing
energy
demands*



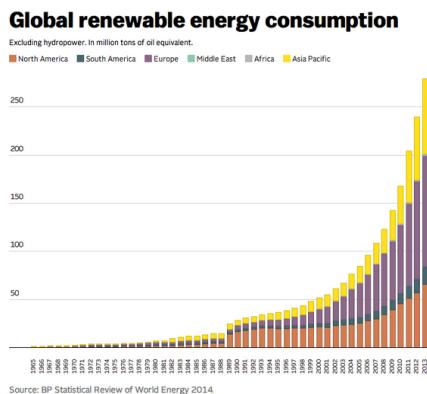
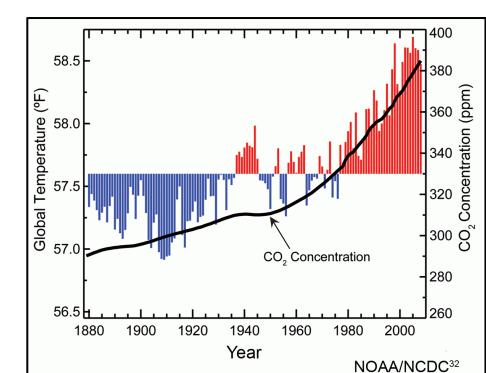
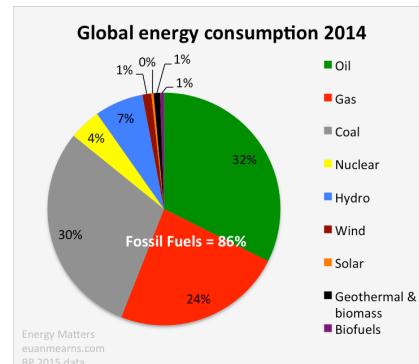
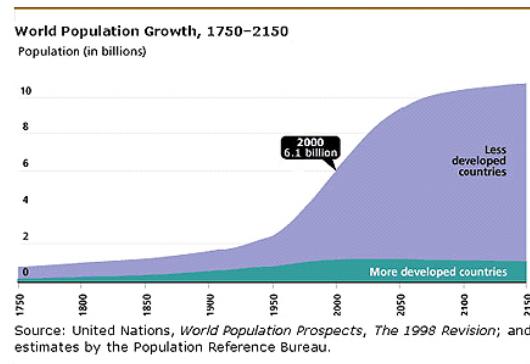
Fossil fuel
consumption



Increase in the
atmospheric
CO₂



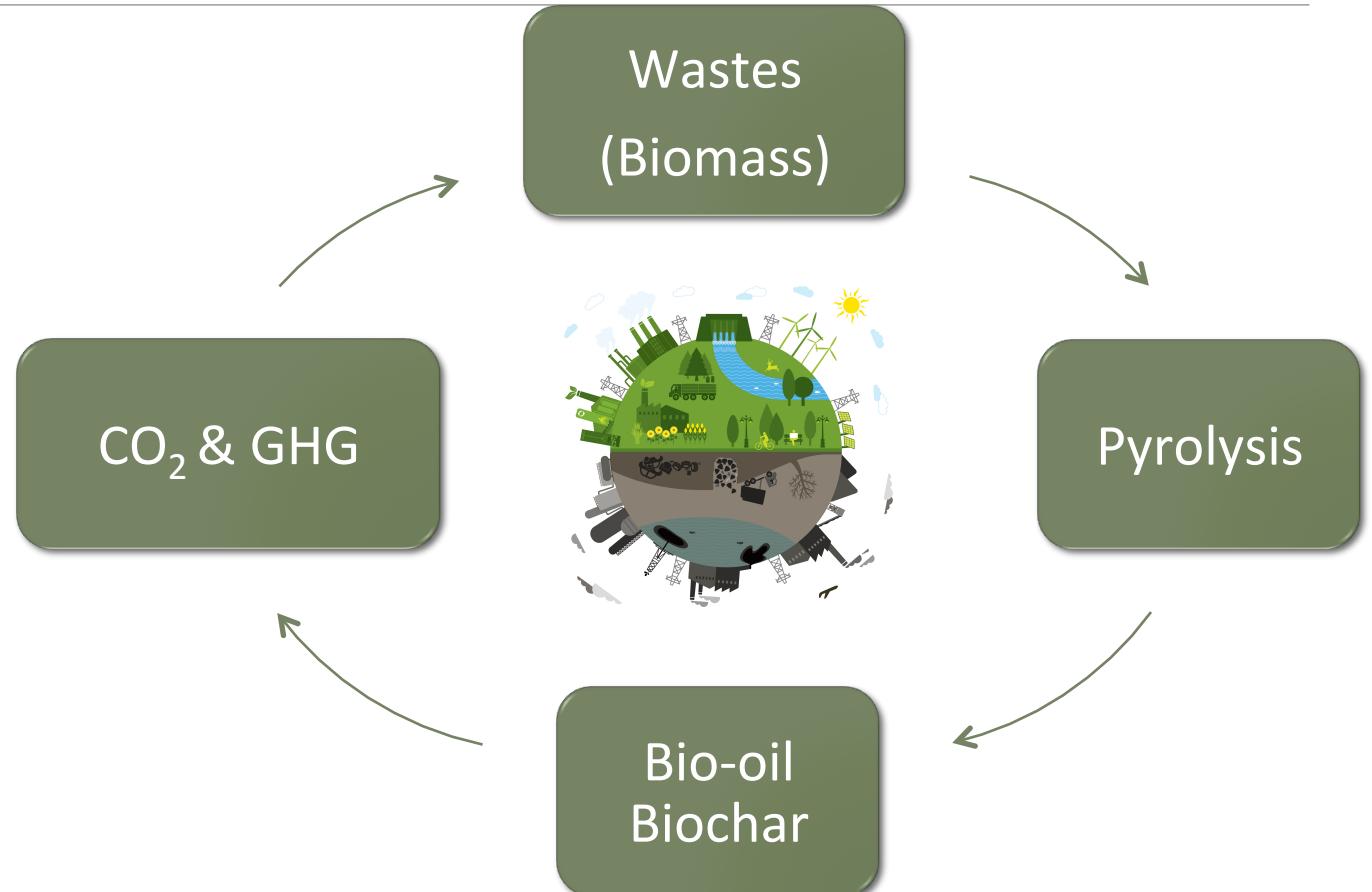
Utilization of
renewables



Objective-Motivation

Utilization of Renewables:

- Solar
- Wind
- Geothermal
- Wave
- Biomass





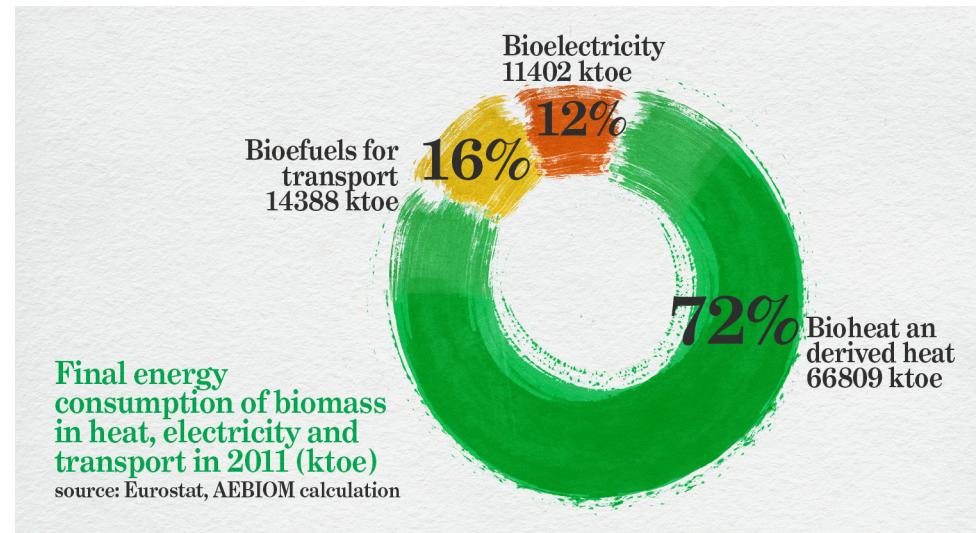
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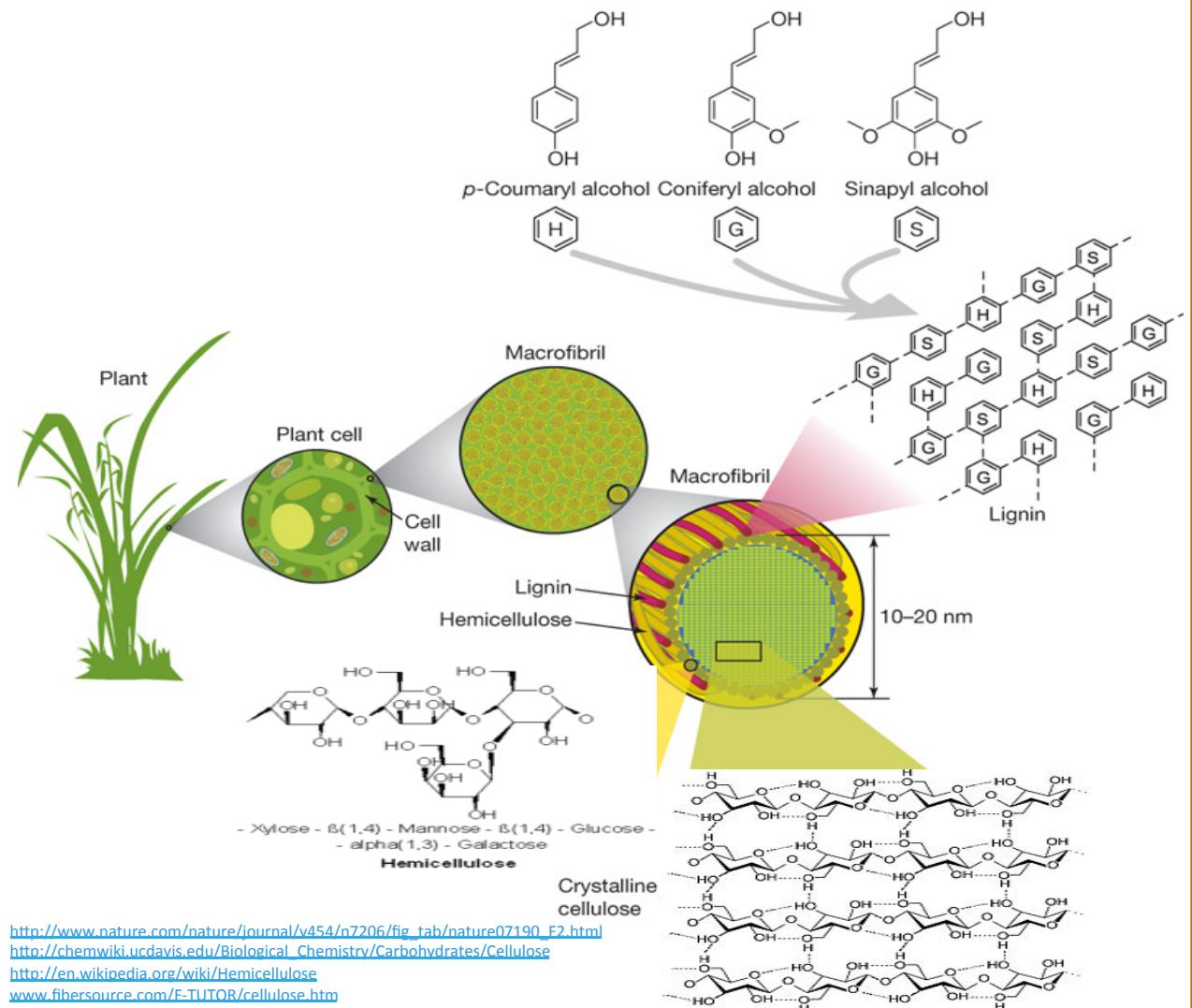


Understanding Biomass

Biomass ??? Waste



Components and thermal degradation of lignocellulosic biomass



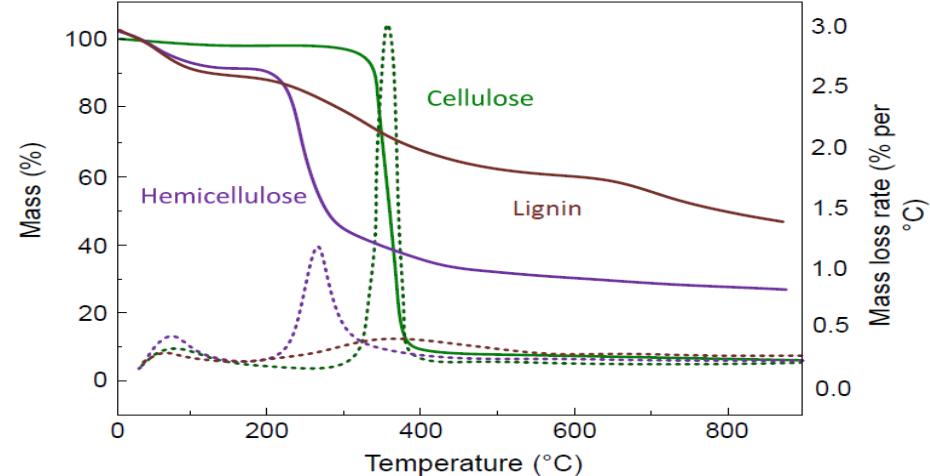
http://www.nature.com/nature/journal/v454/n7206/fig_tab/nature07190_F2.html

http://chemwiki.ucdavis.edu/Biological_Chemistry/Carbohydrates/Cellulose

<http://en.wikipedia.org/wiki/Hemicellulose>

www.fibersource.com/F-TUTOR/cellulose.htm

Mohan et. al., Energy & Fuels, Vol. 20, No. 3, 2006



Hemicellulose

- Thermal decomposition: 200-260 °C
- Produces more volatiles, less tar, and less char than cellulose.

Cellulose

- Thermal decomposition: 200-350 °C
- Produces mainly CO, CO₂, H₂O and lower molecular weight hydrocarbon gases,
- Produces more tar than hemicellulose, less char than lignin.

Lignin

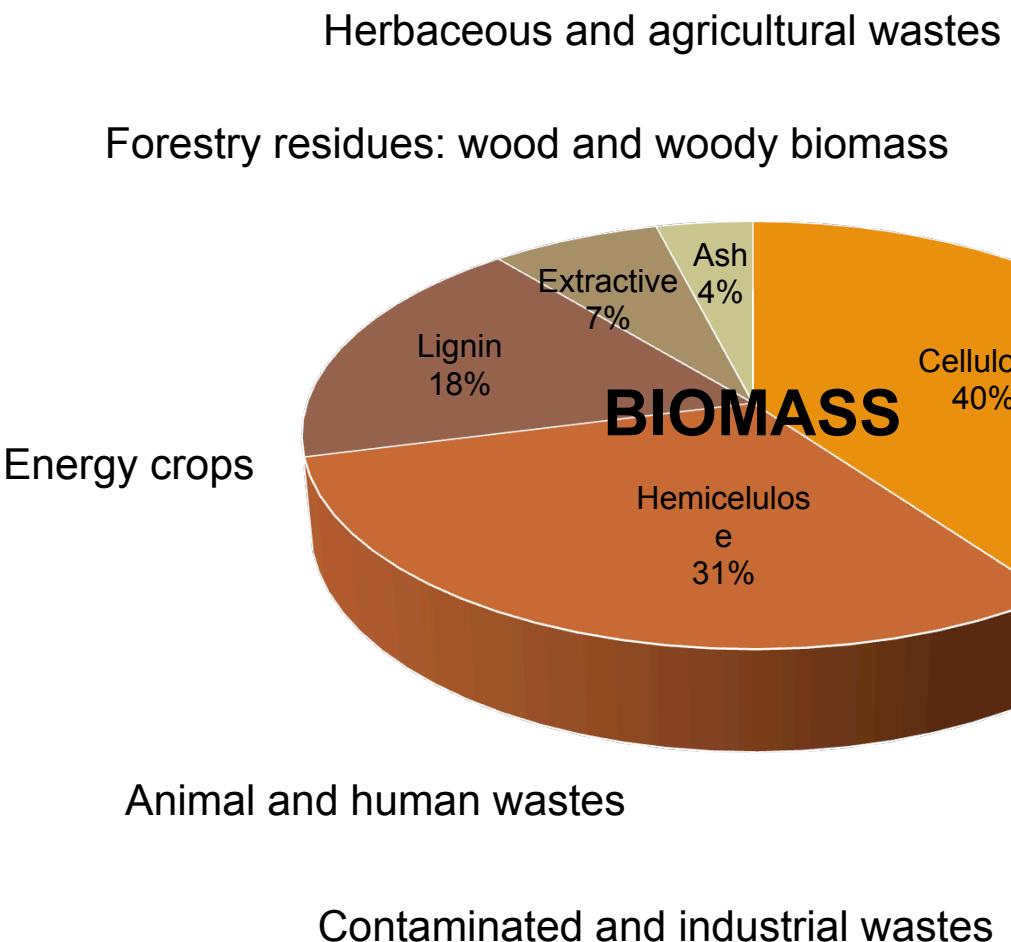
- Thermal decomposition: 230-500 °C.
- Lignin is more difficult to dehydrate than cellulose or hemicelluloses.
- Produces more residual char than does the pyrolysis of cellulose.



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BIOMASS TYPES



THERMOCHEMICAL CONVERSION PROCESSES

PRODUCTS

COMBUSTION → HOT GASES

PYROLYSIS → CHAR

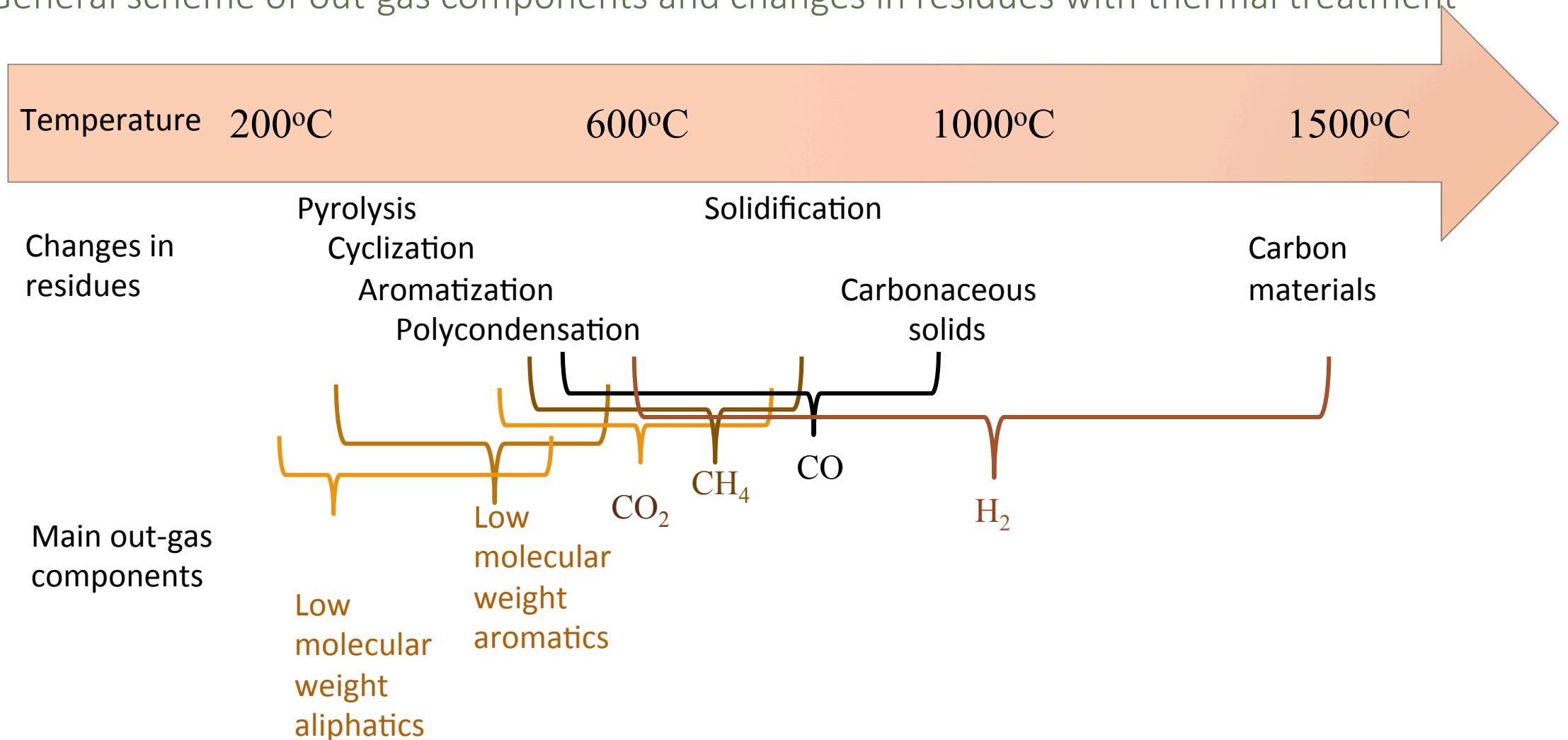
LIQUEFACTION → HYDRO-CARBONS

GASIFICATION → LOW ENERGY GAS

→ MEDIUM ENERGY GAS

Thermal decomposition of biomass

General scheme of out-gas components and changes in residues with thermal treatment



Typical process conditions and product yields for pyrolytic processes

| | Fast pyrolysis | Slow pyrolysis (Carbonisation) | Torrefaction (partial slow pyrolysis) |
|---------------------------------------|--------------------------|--------------------------------|---------------------------------------|
| Temperature | ~ 500°C | > 400°C | < 300°C |
| Heating rate | Fast, up to 1000°C/min | Slow, 5-80°C/min | - |
| Reaction time | Few seconds | Hours to days | < 2h |
| Pressure | Atmospheric (and vacuum) | Atmospheric (or up to 1 MPa) | Atmospheric |
| Medium | Oxygen-free | Oxygen-free or oxygen-limited | Oxygen-free |
| Typical product yields (wt. %) | | | |
| Bio-oil (wt %) | 75 | 30 | 5 |
| Char (wt%) | 12 | 35 | 80 |
| Gases (wt.%) | 13 | 35 | 15 |

Ref.: Ronnse, F. (2016), Bridgwater (2012); van der Stelt *et al.* (2011); Williams and Besler, (1996); Bain and Broer (2011); Nachenius *et al.* (2013); Kambo & Dutta,(2005).



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Bio-oil



Fuels
Hydrogen
Upgrading
Fuel via syngas

Chemicals
Resins
Flavours
Adhesives
Phenolics

Heat
Cofiring of boiler and furnace

Power
Diesel Engine
Turbine

Properties of bio-oil

| Property | Bio-oil | Light Fuel Oil | Heavy Fuel Oil |
|----------------------------------|------------|----------------|----------------|
| Moisture content (wt.%) | 15-30 | - | 0.1 |
| Ash content (wt.%) | <0.02 | <0.01 | 0.03 |
| Specific gravity | 1.2 | - | 0.94 |
| pH | 2-3 | - | - |
| Viscosity at 50 °C (centistokes) | 7 | 4 | 50 |
| Pour point (°C) | -33 | -15 | -18 |
| Distillation residue (wt.%) | <50 | - | <1 |
| Higher heating value (MJ/kg) | 20-30 | 35-37 | 38-40 |
| Elemental composition (wt.%) | | | |
| C | 54-58 | - | 85 |
| H | 5.5-7.0 | - | 11 |
| N | 0-0.2 | 0 | 0.3 |
| S | Negligible | 0.15-0.5 | 0.5-3.0 |
| O | 35-40 | - | 1.0 |

Czernik and Bridgwater, 2004;
Mohan et al., 2006



Effect of process conditions on bio-oil yields for various biomass samples

| Biomass | Pyrolysis Temperature (°C) | Reactor type | Heating rate (°C/min) | Pyrolysis atmosphere | Catalyst | Maximum bio-oil yield (wt.%) | Heating Value (MJ/kg) | Reference |
|-----------------------------------|----------------------------|--|-----------------------|----------------------|---------------|------------------------------|----------------------------|---------------------|
| Pinewood sawdust | 500 | Conical spouted bed reactor | Fast pyrolysis | Nitrogen | -- | 75.0 | 14.6 (Lower heating value) | Amutio et al., 2012 |
| Hard wood or soft wood feedstocks | 450 | Tubular vacuum pyrolysis reactor | Slow pyrolysis | Nitrogen | -- | 50.0-55.0 | -- | Ortega et al., 2011 |
| Rice straw | 550 | Fixed-bed reactor | 5 | Steam | -- | 35.86 | 32.58 | Pütün et al., 2004 |
| Apricot pulp | 550 | Fixed-bed reactor | 5 | Steam | -- | 27.7 | 35.63 | Özbay et al., 2008 |
| Olive residue | 500 | well-swept and high-speed heated fixed-bed batch reactor | 500 | Nitrogen | -- | 46.72 | 29.6 | Pütün et al., 2009 |
| Euphorbia rigida | 550 | Fixed-bed reactor | 7 | Static | Criterion-534 | 30.98 | -- | Ateş et al., 2005 |

Biochar

Slow Pyrolysis and Carbonization

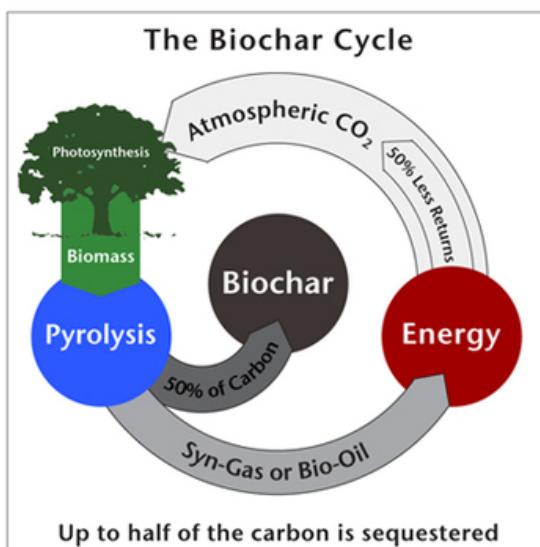
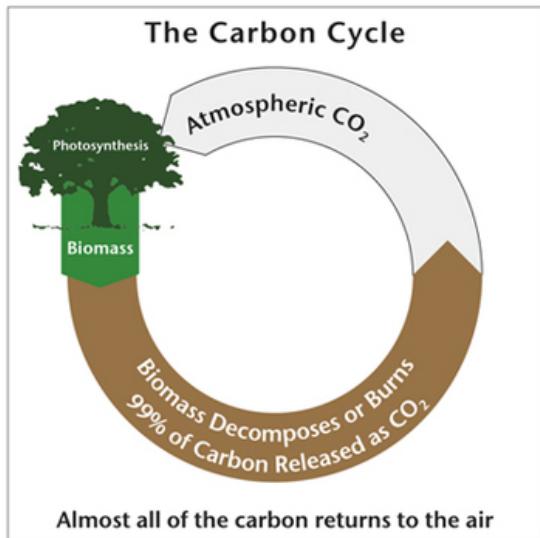
Non-graphitizable carbonaceous solid residue after pyrolysis.

Char

- Solid synthetic fuels
- Bio-oil/char slurry
- Adsorbents
- Substrate for catalysts

Bio-char

- C sequestration
- Soil conditioning via changes in soil chemistry
- Soil amendment



Ref.: Biochar solutions Inc., 2011

Biochar Production: Effect of various parameters

| Parameters | Degree | Expected result |
|-------------------|-------------------------------------|---|
| Feedstock related | Hemicellulose+Cellulose | Low (<55 %) |
| | Lignin | High (>35 %) |
| | Ash | High (>8 %) |
| | Moisture content | Low (<10 %) |
| | Particle size | Low (< 2 mm) |
| Process related | Batch | - |
| | Continuous | - |
| | Heating rate | Low (< 10°C/min) High (> 300°C/min) |
| | Pyrolysis/Carbonization Temperature | Low (<400 °C) Moderate (~500 °C) High (>700 °C) |
| | Residence Time* | Low (0<t<10 min) High (>1 h) |

* Residence time refers to the holding time of biochar at the final pyrolysis temperature.



Biochar Production: Examples from previous studies

| Biomass type | Reactor type | Biochar production techniques | Biochar production temperature (°C) | Heating rate (C min ⁻¹) | Reaction time (min) | Yield (%) | C (wt. %) | Surface area m ² g ⁻¹ | Reference |
|-----------------|---------------------------|-------------------------------|---|---|--|--|-------------------------|---|-------------------------------|
| Pine Cone | Fixed-bed reactor | Slow pyrolysis | 550 | 10 | -- | 29.6 | 95.16 | 208 | Apaydin-Varol and Pütün, 2012 |
| Soybean Cake | | | | | | 25.2 | 83.95 | 2.1 | |
| Corn Stalk | | | | | | 24.9 | 94.97 | 11.8 | |
| Peanut Shell | | | | | | 29.7 | 93.61 | 211 | |
| Tea Waste | Fixed-bed tubular reactor | Fast pyrolysis | 400 500 550 700 | 300 300 300 300 | 10 | 43.4 35.7 30.2 21.1 | -- | 2 - - 7.5 | Uzun et al., 2010 |
| Pistachio shell | Fixed-bed tubular reactor | Fast/slow pyrolysis | 400 500 550 700 500 500 500 | 300 300 300 300 100 500 700 | 21.7 20.5 15.4 28.0 24.7 22.0 20.9 | 29.5 20.5 15.4 28.0 24.7 22.0 20.9 | -- -- -- | -- -- -- | Pütün et al., 2007 |
| Olive residue | Fixed-bed reactor | Slow pyrolysis | 400 500 550 700 | 7 | -- | 32.4 28.8 28.0 27.5 | -- 69.34 -- -- | -- -- -- | Pütün et al., 2005 |
| Rice straw | Fixed-bed reactor | Slow pyrolysis | 400 500 550 700 | 5 | -- | 30.5 27.6 26.1 23.6 | -- -- -- -- | -- -- -- -- | Pütün et al., 2004 |

Biochar Characterization

- The International Biochar Initiative (IBI) biochar standards identify three categories (A, B and C) of tests for biochar materials.

- Category **A** and Category **B** are for basic utility properties and toxicant reporting.
- Necessary for all biochars.

- particle size and moisture
- elemental composition (H, C and N)
- ash proportion
- electrical conductivity
- pH/liming ability.
- the soil toxicity assessment thresholds.

- The category **C** is optional and composed of advanced analysis and soil enhancement indicators.

- volatile matter content
- nutrient content
- surface area

- Other techniques recently studied...

- Surface morphology
- porosity
- Surface chemistry-functional groups
- CEC
-

General experimental procedure



Feedstock

Oven dried
and sieved



Pre-analysis

Ultimate,
Proximate,
TGA_FTIR_MS
and Component
analysis,
ICP-OES



Slow Pyrolysis

400, 450,
500, 550 and
600 °C 10
°C/min, 30
min residence
time



Bio-oil

Separation to
subfractions,
transportation
fuels,
Phenolic
compounds



Biochar

High
nutrient
capacity,
Microporosit
y, Alkaline
and Carbon
structure



Biochar Analysis

CHN
analysis, pH,
SEM, He
pycnometer,
ICP-OES



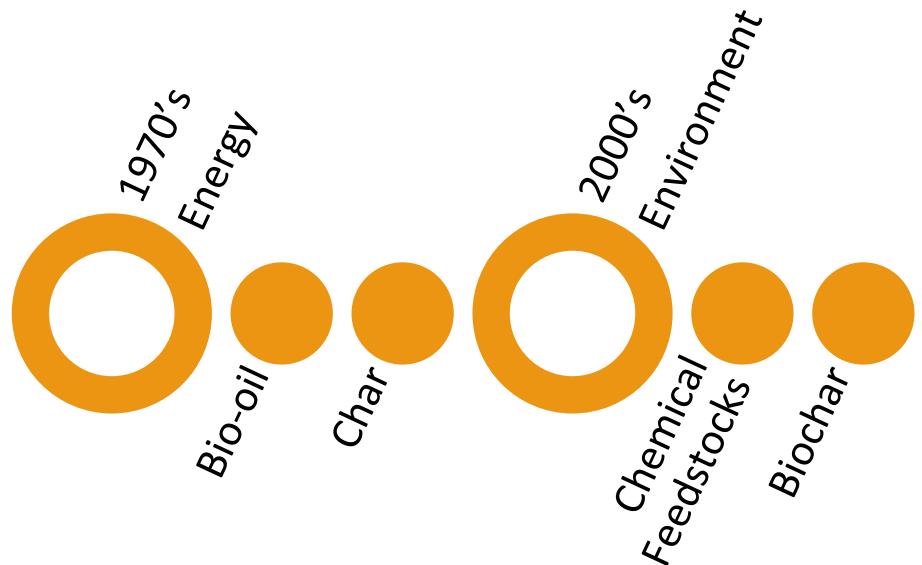
Soil

Nutrient release,
Contaminant
adsorption, C
sequestration,
pH neutralizing



Conclusions and further remarks

Pyrolysis - Where are we now???



Pyrolysis – What is next???

Diversity of biomass samples and accordingly bio-oil and bio-char properties emphasises the need for a case-by-case evaluation of each product prior to its utilization.

Last year Prof. Basak Burcu Uzun passed away unexpectedly.
We have not only lost a colleague but a true friend.



Thank you for your
attendance...

For more contacts:
eapaydin@anadolu.edu.tr